



## Case Study: Thickening solutions

### Vane Feedwell™ – significant improvements in underflow density, flocculant cost and operability at Tiwest's North Mine Concentrator

**Organisation:** Tiwest

**Site:** Cooljarloo, Western Australia

**Year:** 2008

**Application:** ■ Mineral sands

**Project:** ■ Thickener feedwell retrofit

**Solution:** ■ Vane Feedwell™

**Results:**

- Project delivered on time, on budget
- Increased underflow density by 2%
- Reduced flocculant costs by 20%
- Increased water recovery
- More stable thickener operation

Tiwest is the world's largest integrated titanium minerals production and manufacturing company and is a joint venture company between Tronox and Exxaro Sands. The company mines from shoreline deposits approximately 170 km north of Perth in Western Australia, at its Cooljarloo Mine. Tiwest produces more than 700,000 tonnes of heavy mineral concentrate (HMC) a year from strand lines, using both a dredging operation and dry mining techniques.

#### Project overview

The dry mine, or North Mine Concentrator as it is known, uses earth moving equipment to extract ore located above the water table, feeding it to the land-based concentrator for separation of the heavy minerals from the sand and clay using a series of gravity spirals. The dry mine feeds clay residue (slimes) to an Outotec High Compression Thickener. The 20m diameter thickener incorporates a feed dilution system using both forced dilution and self-dilution. The thickener was designed to a duty of 80 t/hr and a feedwell volume flow of 1500 m<sup>3</sup>/hr, based on 3% w/w feedwell solids.

**Outotec**  
More out of ore

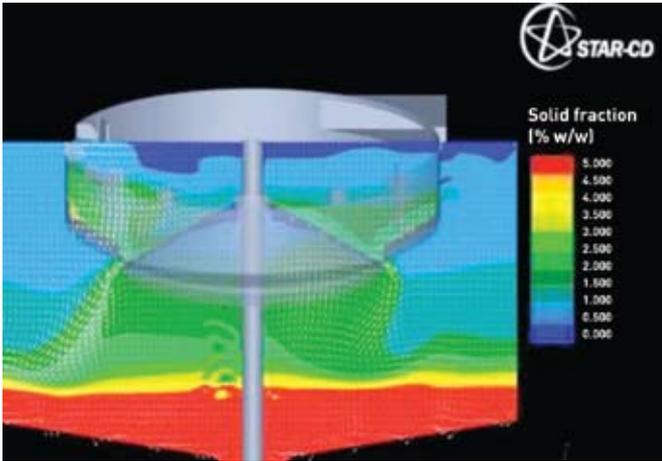


Figure 1: Elevation view of flow pattern and solids concentration in unmodified feedwell

In July 2006 feed material characteristics changed and thickener performance subsequently declined. The feed differed considerably in mineralogy from previous material and also was heterogeneous in nature. As a result of this new feed material, thickener flocculant dose increased, underflow density reduced and overflow sliming/pulping occurrences increased. All this led to poor thickener performance, with significant water losses and slimes dam capacity impacts.

Tiwest approached Outotec to assist with improving the performance of the thickener. The newly developed Vane Feedwell™ was put forward as an option to resolve the thickener issues affecting the North Mine Concentrator.

Vane Feedwell™ components were retrofitted to the internals of the existing feedwell. The components include vanes, a radially sloped shelf and directional auto dilution, all now standard Outotec Vane Feedwell™ design features.

### Computational Fluid Dynamics (CFD)

Outotec's CFD thickening team in Perth modelled the feedwell performance before and after the Vane Feedwell™ retrofit. Eulerian-Eulerian multiphase CFD was used with buoyancy included to correctly incorporate density effects. The  $\kappa$ - $\epsilon$  turbulence model was applied with a mesh of ~1.6 million nodes, grouped predominantly in the feedwell region. The following section highlights some of the key modelling carried out by Outotec's CFD thickening team.

### Flow pattern

Figures 1 and 2 show an elevation view of the flow pattern and solids concentration in the unmodified and retrofitted feedwell. It is immediately obvious that the retrofitted Vane Feedwell™ has much better solids retention, with the majority of the feedwell solids close to the desired 3 % w/w for optimal flocculation. The shelf and vanes have held the feed stream up in the top half of the feedwell and the swirl is maintained right the way around the surface, ensuring effective feed solids and flocculant distribution and mixing. By comparison, the unmodified feedwell has virtually no solids in the top half of the feedwell, with this zone being bypassed and not effectively utilised for flocculation.

### Shear

Shear is a natural by-product of turbulence dissipating the feed momentum/kinetic energy, and it is also a critical factor in flocculation. Turbulence provides mixing, both of feed and

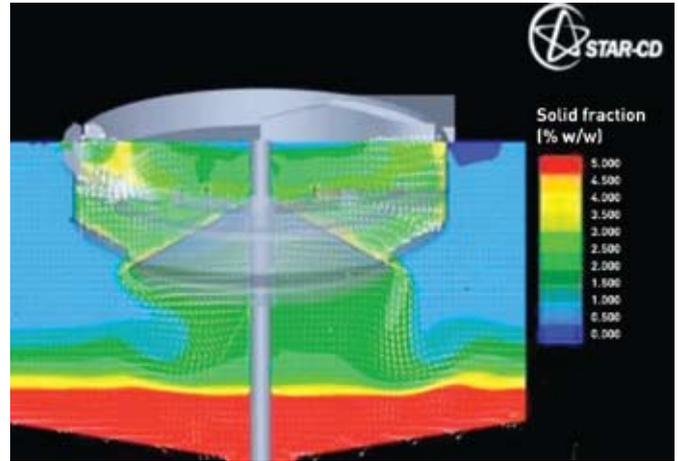


Figure 2: Elevation view of flow pattern and solids concentration in Vane Feedwell™

dilution liquor, but also flocculant and feed slurry. Ideally, shear rates should be moderate in the top of the feedwell where the flocculant is added, and then lower in the bottom zone to ensure the aggregates safe exit.

Figure 3 shows the unmodified feedwell, with figure 4 displaying the improvements from the Vane Feedwell™ retrofit. Without it, the shear rates are essentially too low throughout the feedwell.

Fitting the Vane Feedwell™ components improves this situation considerably. There are higher shear rates in the top of the feedwell which, when associated with the better solids retention in this area, will result in improved flocculation and better feed momentum dissipation. Finally, the shear rates are decreased in the exit region, indicating a reduction in flocculated aggregate breakage when discharging into the thickener body.

### Tiwest thickener upgrade

Tiwest undertook the thickener upgrade at their North Mine in May 2008 to coincide with an extended plant shut down. In addition to the new Vane Feedwell™, an improved flocculant addition arrangement, enhanced instrumentation and new static and upright rake pickets were installed to improve underflow densities.

### Process results

Process data was taken, both pre and post Vane Feedwell™ retrofit, from online instrumentation. Laboratory flocculant demand is also included, as this is Tiwest's own internal characterisation of the slimes feeding the thickener. This has been used as a reference to determine if ore variability impacted the results.

### Thickener flocculant dose

Slimes thickener flocculant dose prior to the retrofit was averaging 490 g/t, with a standard deviation of 114 g/t. Post installation flocculant dose reduces by approximately 20% to an average of 393 g/t and process stability occurs with a standard deviation of only 12 g/t.

From an operational perspective, the reduction in flocculant consumption is estimated to be primarily as a result of the new feedwell, with contributions also from the improved flocculant addition arrangement, pickets and instrumentation.

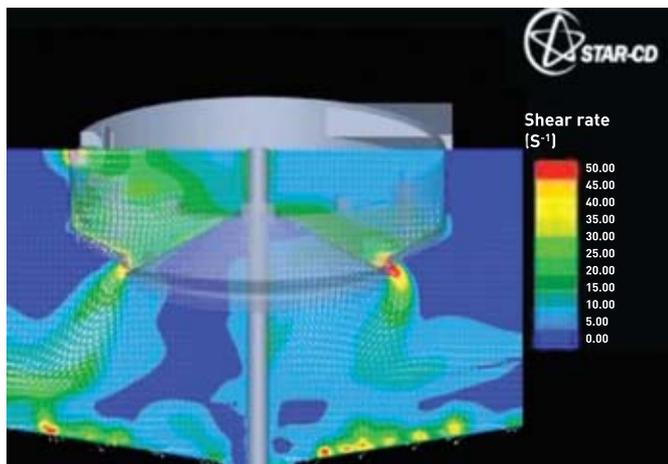


Figure 3: Elevation view of flow pattern and shear rate in unmodified feedwell

### Thickener underflow density

Underflow density shows a major difference post Vane Feedwell™ installation. Prior to the retrofit, the slimes underflow density averaged 18% w/w with a standard deviation of 3.7% w/w. Post retrofit, a density of 20% w/w was averaged, perhaps more interesting, with a standard deviation of only 1.2% w/w. This implies that not only a higher underflow density can be achieved but also more consistently, resulting in improved process operability. This again highlights the Vane Feedwell's ability to smooth out process variability and hence operate across a wider range. It is believed the addition of rotating pickets also helped underflow density.

Underflow density increase enables slimes deposition to be maximised. This is a very important factor for both Tiwest's operating costs and sustained operation, since the water lost to thickener underflow is evaporated in slimes cells and lost from the process. Tiwest had experienced plant shutdowns due to mine site water shortages during the summers of 2007 and 2008.

### Thickener underflow throughput

Thickener underflow tonnage rates are fairly constant across the time period at approximately 60 t/h, indicating that feed rates are not significantly different pre and post installation. Feed rates therefore do not bias the data one way or the other.

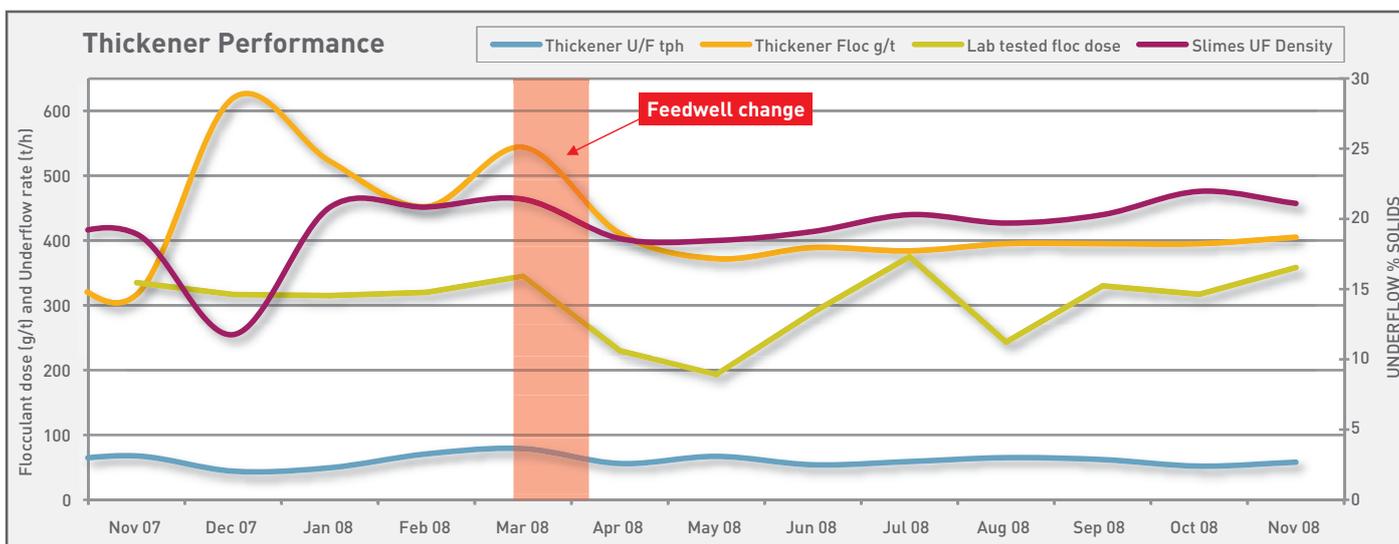


Figure 5 – Thickener trends pre and post Vane Feedwell™ retrofit

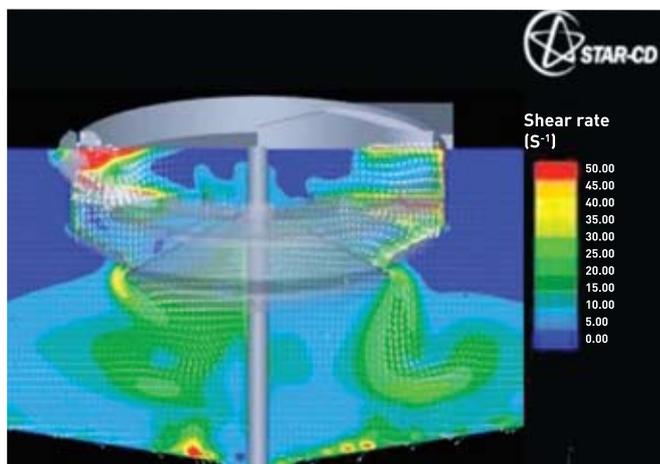


Figure 4: Elevation view of flow pattern and shear rate in Vane Feedwell™

### Flocculant demand

Flocculant dose, as determined through Tiwest's laboratory characterisation procedure, can be viewed as being essentially consistent at an average of 300 g/t both pre installation and post. The variability in laboratory flocculant demand needs to be viewed against the actual thickener flocculant dose and the other variables to compile a total picture.

Of particular interest is a comparison of the laboratory flocculant demand versus the actual thickener dose. During the post installation period, despite varied laboratory flocculant demand, actual thickener dose is very stable. This indicates that the Vane Feedwell™ has the ability to operate across a range of conditions and also is less sensitive to changes in flocculant demand requirements.

### “A great success...”

Coupled with the plant data are the visual observations and experiences from Cooljarloo site personnel. The following is a direct quote:

“My observation was that the thickener modifications had an immediate impact on thickener performance. Underflow density increased immediately and since the installation we have had very few thickener issues. From my perspective the project was a great success as we have had very little reduced throughput or downtime due to thickener performance since the modifications were put in.” – Terry Tye, North Mine Superintendent.

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**Outotec Pty Ltd**

1/25 Frenchs Forest Road  
Frenchs Forest NSW 2086  
Tel: +61 2 9984 2500  
Fax: +61 2 9984 2501

Level 2, 1 Walker Ave  
West Perth WA 6005  
Tel: + 61 8 9211 2200  
Fax: +61 8 9211 2201  
Email: [minpro.australia@outotec.com](mailto:minpro.australia@outotec.com)  
Website: [www.outotec.com](http://www.outotec.com)

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